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POLLUTION CONTROL

Polluted air and other gases can be purified by heat treatment to such temperatures that the pollutants are oxidised or decomposed. US patent 4 267 152 and US patent 4 741 690 describes such processes where the polluted 5 gases are fed through regenerative devices where the heating of a gas is immediately followed by cooling and recovery of the heat content of the gas. In this way heat treatment of the gas to a high temperature can be made in an economical way without a high expenditure of energy.

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The incoming raw gas is in these processes successively heated to the high temperature by means of contact with a matrix of solid material capable of heat transfer to the gas. In the solid matrix there is a temperature gradient 15 so that the gas is first successively heated to a maximum temperature. After attaining its maximum temperature the gas is then cooled in an analogous manner by means of contact with a solid matrix of successively lower temperature. In US patent 4 287 152 the heating and the 20 cooling matrices are separated from each other but used alternatively for heating and cooling purposes according to an alternating direction of gas flow through the matrices. The different matrices are alternatively used for heating and cooling of the gas. In US patent 4 741 25 690 there is only one continuous matrix through which the gas flow is being fed. The temperature profile in this matrix is such however that when the gas passes through it is first successively heated to a maximum temperature and then successively cooled.

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In both cases the operation is regenerative and the gas is fed in alternating directions through the equipment and is successively first heated to a maximum temperature and then cooled. The maximum temperature employed is such 5 that it is at or above the temperature that is necessary for the intended oxidation or decomposition reaction to take place.

Processes and equipment like these are extensively used 10 for the purification of ventilation air from painting and printing processes. It can also be used for the purification of exhaust gases from internal combustion engines. In this and other cases nitrogen oxides are a part of the pollution problem.

15 For diesel engines the concentration of nitrogen oxides in the exhaust can reach several thousands of ppm. Good reduction of these nitrogen oxides can be accomplished if the exhaust is first mixed with a corresponding amount of 20 ammonia, urea or other amine compound before it is heat treated in the above described manner. During the heating the mixture will pass through the relevant temperature window for a selective non catalytic reduction (SNCR) reaction where the nitrogen oxides and the amines are 25 transformed to elemental and harmless nitrogen.

Diesel engine exhaust for example can thus be purified in the above described process first during the heating phase when nitrogen oxides are removed and then at the 30 high temperature when soot, aldehydes and other organic matter is oxidised. This way of operation of the equipment is described in European patent number EPC 609 288.

Experience has shown that when the original concentration of nitrogen oxides is more than 1000 ppm a good reduction can be achieved and the concentration nitrogen oxides brought down to a couple of hundred ppm. However when the 5 original concentration already is in this low region as for example in the exhaust from lean burn natural gas engines reduction is very poor.

The present invention constitutes a way of improving this 10 situation so that the concentration of nitrogen oxides in the outgoing treated gas can be brought down significantly below 50 ppm. The improvement is accomplished by the incorporation of catalytically active zones into the heat transfer matrices of earlier designs.

15 An embodiment of the invention is described in figure 1 and another embodiment of the invention is described in figure 2. In both figures 1 is a valve mechanism for the direction of air (gas) in alternating directions through the equipment. 2 and 3 are connecting ducts for incoming raw and outgoing cleaned gas respectively. 4 and 5 are wind boxes for distribution and collection of air (gas) that goes through the heat transfer matrix 6. In the 20 design shown in figure 2 this matrix is divided into two parts 6 and 6' surrounding a combustion chamber 7 which is absent in the design shown in figure 2 where the heat exchanging matrix stretches all the way between the two wind boxes 4 and 5. Both designs comprises means for 25 heating: in figure 1 in the form of electric heaters 8 and in figure 2 in the form of a burner 9. Both designs also incorporate catalytically active zones 10 and 11 within the heat exchanging matrices. In the design of 30 figure 1 the temperature is high in the centre of the heat exchanging matrix 6 and gradually decreases towards the top and bottom. In the design in figure 2 the temperature 35

is high in the combustion chamber 7 and the upper parts of the heat exchanging matrixes 6 and 6' and the temperature gradually decreases towards the bottom of the heat exchanging matrices. By regenerative heat exchange and 5 regular switching of the direction of flow through the equipment these temperature patterns can be generally maintained without excessive heat demands being put on the heating means 8 (figure 1) and 9 (figure 2). When the oxidation of pollutants in the gas stream produces enough 10 energy they can be switched off altogether.

In operation raw polluted gas is first mixed with ammonia, urea, or other compound able to act as a 15 selective nitrogen oxides reducing agent. The mixture is then introduced into a cold end of a heat exchanger matrix and by passing through it is successively heated to oxidation or decomposition temperature which is attained in the inner part of the equipment i.e. the hot 20 centre of the matrix in fig 1 or the uppermost parts of the matrixes 6 and 6' and the combustion chamber 7 in fig 2. Before reaching this high temperature however the mixture is passed through the catalytically active zone 25 of the heat exchanger matrix 6 or 6'. Here nitrogen oxides react with the mixed in reducing agent and are thus removed. The catalytic zone is placed in the heat exchanging matrix in such a way that the temperature conditions there are favourable for this reduction and a selective catalytic reaction (SCR) takes place. The 30 reaction takes place at a substantially lower temperature than an SNCR reaction and this together with the use of catalyst makes a more thorough reduction possible as compared with an operation according to European patent EPC 609 288 and lower levels of concentration of nitrogen 35 oxides are obtainable. When the inlet concentration of

nitrogen oxides is low the difference becomes significant.

After the SCR reaction the gas mixture is further heated  
5 and as in European patent EPC 609 288 other pollutants as  
well as any remaining surplus of reduction agents are  
destroyed in the hot inner part.

In operation of regenerative equipment like this the  
10 direction of gas through the equipment is reversed at  
regular intervals. Unless special precautions are taken,  
at every change in flow direction some untreated gas  
mixture is being "short circuited" or carried over to the  
outlet. It is then advantageous to interrupt the supply  
15 of reducing agent for a short period before such changes  
in flow direction. Unnecessary emissions of reducing  
agent is then avoided.

An important aspect of the invention is that catalyst can  
20 be applied in such a way that the reducing activity of  
the catalyst is retained for a considerable time after  
the supply of reducing agent has been interrupted. The  
overall reduction efficiency of the equipment thus is not  
disadvantageously affected by such interruptions in the  
25 supply of reducing agent. This effect can be so  
pronounced that the equipment can be modified to comprise  
only one zone of catalytically active material. This zone  
is then activated by the supply of reducing agent when  
this part of the equipment is used as inlet end for the  
30 gas stream. When the gas stream is reversed and the  
active zone is at the outlet end of the equipment the  
supply of reducing agent is cut off and the reduction of  
nitrogen oxides takes place in this zone after the high  
temperature treatment. Figure 3 shows such a design with  
35 only one catalytically active zone 10.

The invention has been described above in the conjunction with regenerative equipment using either one heat exchanging matrix or two different matrices surrounding a combustion chamber. There also are designs using three or 5 more heat exchanging matrices surrounding a common combustion chamber. In some designs the direction of flow through the heat exchanging matrix is changed only gradually in the heat exchanging matrix so that different parts of the same matrix have flow in different directions. This is obtained for instance by rotation of a 10 matrix versus fixed inlet and outlet ports or by the use of a rotating valve system working together with a fixed matrix. Together all these different designs are often 15 called regenerative thermal oxidisers (RTOs). In all the different designs the heat exchanging matrix material is subject to a gas flow that is reversed at regular intervals and the incoming gas is successively heated to a high temperature where oxidation and decomposition takes place. The invention is applicable in all these cases. 20 The design shown in figures 1 and 3 have the advantage that the equipment is compact and can be made comparatively small which very often is an important aspect when used in various conjunctions together with internal combustion engines.

25 Catalytically active zones can be incorporated in at least one of the matrices and be activated by regular supply of reducing agent. As described above this supply does not have to be continuous. In some cases the raw gas 30 may already contain such reducing agents or the catalyst or combination of catalyst and raw gas be such that no such supply is necessary.